

# Equations of Fluid Dynamics

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## 1. Euler Equations

A system of non-linear hyperbolic conservation laws that govern the dynamics of a compressible material, for which the effects of body forces, viscous stresses and heat flux are neglected.

Set of variables to describe the flow can be chosen:

- primitive variables: density  $\rho$ , pressure  $p$  and velocity  $\underline{v}$
- conserved variables: density  $\rho$ , momentum  $\rho \underline{v}$ , total energy per unit mass  $E$

Conservation laws:

$$\frac{\partial \underline{U}}{\partial t} + \frac{\partial \underline{F}(\underline{U})}{\partial x} + \frac{\partial \underline{G}(\underline{U})}{\partial y} + \frac{\partial \underline{H}(\underline{U})}{\partial z} = 0 \quad [1]$$

with

$$\underline{U} = \begin{bmatrix} \rho \\ \rho u \\ \rho v \\ \rho w \\ E \end{bmatrix} \quad \underline{F} = \begin{bmatrix} \rho u \\ \rho u^2 + p \\ \rho uv \\ \rho uw \\ u(E+p) \end{bmatrix} \quad \underline{G} = \begin{bmatrix} \rho v \\ \rho uv \\ \rho v^2 + p \\ \rho vw \\ v(E+p) \end{bmatrix} \quad \underline{H} = \begin{bmatrix} \rho w \\ \rho uw \\ \rho vw \\ \rho w^2 + p \\ w(E+p) \end{bmatrix}$$

or in short:

$$\underline{U} = \begin{pmatrix} \rho \\ \rho \underline{v} \\ E \end{pmatrix}; \quad \underline{F} = \begin{pmatrix} \rho \underline{v} \\ \rho \underline{v} \otimes \underline{v} + p \delta_{ij} \\ \underline{v}(E+p) \end{pmatrix} \quad \text{with} \quad \frac{\partial \underline{U}}{\partial t} + \underline{D} \cdot \underline{F} = 0$$

$$E = \rho \left( \frac{1}{2} \underline{v}^2 + e \right); \quad \underline{v} = (u, v, w)$$

total energy per unit mass

$$\frac{1}{2} \underline{v}^2 = \text{specific kinetic energy}; \quad e = \text{specific internal energy}$$

Any set of PDEs written in the form [1] is called a system of conservation laws in differential form.

However, these PDEs are insufficient to completely describe the physical processes involved. There are more unknowns than equations, closure relations are required.

### Equations of state:

$$\text{thermally ideal gases: } T = \frac{p v}{R}$$

$$\text{calorically ideal gases: } e = \frac{p v}{\gamma - 1} = \frac{p}{\rho(\gamma - 1)}$$

## 2. Viscous Stresses

To introduce viscous stresses, the momentum equation of the Euler equations. The stresses in a fluid, given by tensor  $\underline{S}$ , are due to the effects of pressure and viscosity:

$$\underline{S} = -p \underline{I} + \underline{\Pi} \quad \underline{\Pi}: \text{viscous stress tensor}$$

Newtonian approximation:  $\underline{\underline{\Pi}}$  is related to the derivatives of the velocity field  $\underline{\underline{v}}$  via the deformation tensor

$$\underline{\underline{D}} = \begin{bmatrix} u_x & \frac{1}{2}(v_x + u_y) & \frac{1}{2}(w_x + u_z) \\ \frac{1}{2}(u_y + v_x) & v_y & \frac{1}{2}(w_y + v_z) \\ \frac{1}{2}(u_z + w_x) & \frac{1}{2}(v_z + w_y) & w_z \end{bmatrix}$$

with  $u_x = \frac{\partial u}{\partial x}$

or:  $D_{ij} = \frac{1}{2} \left( \frac{\partial v_j}{\partial x_i} + \frac{\partial v_i}{\partial x_j} \right)$

Such that

$$\underline{\underline{\Pi}} = 2\eta \underline{\underline{D}} + \left( \eta_b - \frac{2}{3}\eta \right) (\text{div } \underline{\underline{v}}) \underline{\underline{I}}$$

with  $\eta$ : coefficient of shear viscosity

$\eta_b$ : coefficient of bulk viscosity,  $= 0$  for monoatomic gases

Sutherland formula:  $\eta = C_1 \left[ 1 + \frac{C_2}{T} \right]^{-1} \sqrt{T}$

The Navier-Stokes equations, modified Euler equations, can be written in differential conservation form:

$$\frac{\partial}{\partial t} (\rho \underline{\underline{v}}) + \underline{\underline{\nabla}} \cdot (\rho \underline{\underline{v}} \otimes \underline{\underline{v}} + p \underline{\underline{I}} - \underline{\underline{\Pi}}) = \underline{\underline{0}}$$

### 3. Heat Conduction

Influx of energy contributes to the rate of change of total energy  $E$ . Let  $\underline{Q} = (q_1, q_2, q_3)$  be the energy flux vector, which results from

- i) heat flow due to temperature gradients
- ii) diffusion processes in gas mixtures
- iii) radiation

Consider only heat flow due to temperature gradients:

$$\underline{Q} = -\kappa \underline{\nabla} T, \quad \kappa: \text{thermal conductivity}$$

Similarity to viscosity: Prandtl number

$$Pr \equiv \frac{c_p \eta}{\kappa} = \frac{4\gamma}{3\gamma - 5} = \text{constant}^*$$

The energy equation is then:

$$\frac{\partial E}{\partial t} + \underline{\nabla} \cdot (\underline{v}(E+p)) = -\underline{Q}$$

\* assuming that specific heat at constant pressure  $c_p$  is constant

## 4. Integral Form of Equations

Problem: Differential forms assume smoothness, thus don't allow discontinuous solutions like shocks.

Define substantial/material/Lagrangian/comoving derivative:

$$\text{scalar } \varphi(\underline{x}, t): \frac{D\varphi}{Dt} = \frac{\partial\varphi}{\partial t} + \underline{v} \cdot \underline{\nabla}\varphi$$

$$\text{vector } \underline{v}(\underline{x}, t): \frac{Dv_i}{Dt} = \frac{\partial v_i}{\partial t} + \underline{v} \cdot (\underline{\nabla} v_i) \quad \text{componentwise}$$

$$\frac{Dv_i}{Dt} = \frac{\partial v_i}{\partial t} + v_j \frac{\partial}{\partial x_j} v_i$$

To derive the integral form of the equations, we will need the Reynold's transport theorem:

Let  $I = \int_{V(t)} \alpha d^3x$  be the integral form of an equation, where  $\alpha$  is any scalar, vector or tensor field. Then:

$$\frac{dI}{dt} = \frac{d}{dt} \left[ \int_{V(t)} \alpha d^3x \right] = \int_{V(t)} \left[ \frac{\partial \alpha}{\partial t} + \underline{\nabla}(\alpha \cdot \underline{v}) \right] d^3x$$

Proof: Let  $V(t)$  be some finite volume with  $dV(t=0) = dV_0$ . Furthermore, let  $\varphi(\underline{x})$ :

$$\varphi(\underline{x}) = \begin{cases} 1 & \underline{x} \in V(t) \\ 0 & \text{else} \end{cases}$$

$$\text{such that } I = \int_{V(t)} \alpha d^3x = \int_{\mathbb{R}^3} \alpha \varphi d^3x$$

to move the time dependence of the volume into the integral.

By definition:  $\frac{D\varphi}{Dt} = \frac{\partial\varphi}{\partial t} + \underline{v} \cdot \underline{\nabla}\varphi = 0$  because  $\varphi$  is comoving.

$$\begin{aligned} \text{Then: } \frac{dI}{dt} &= \frac{d}{dt} \left[ \int_{V(t)} \alpha d^3x \right] = \frac{d}{dt} \left[ \int_{\mathbb{R}^3} \alpha \psi d^3x \right] = \int_{\mathbb{R}^3} \frac{d}{dt} [\alpha \psi] d^3x \\ &= \int_{\mathbb{R}^3} \left[ \frac{d\alpha}{dt} \psi + \alpha \frac{d\psi}{dt} \right] d^3x \end{aligned}$$

$$\text{Using } \frac{D\psi}{Dt} = 0 \Rightarrow \frac{\partial \psi}{\partial t} = -\underline{v} \cdot \underline{\nabla} \psi$$

$$\Rightarrow \frac{dI}{dt} = \int_{\mathbb{R}^3} \left[ \frac{\partial \alpha}{\partial t} \psi - \alpha \underline{v} \cdot \underline{\nabla} \psi \right] d^3x$$

$$\text{Using } \underline{\nabla} \cdot (\psi \alpha \underline{v}) = \psi \underline{\nabla} \cdot (\alpha \underline{v}) + \alpha \underline{v} \cdot \underline{\nabla} \psi$$

$$\Rightarrow -\alpha \underline{v} \cdot \underline{\nabla} \psi = \psi \underline{\nabla} \cdot (\alpha \underline{v}) - \underline{\nabla} \cdot (\psi \alpha \underline{v})$$

$$\Rightarrow \frac{dI}{dt} = \int_{\mathbb{R}^3} \left[ \frac{\partial \alpha}{\partial t} \psi + \psi \underline{\nabla} \cdot (\alpha \underline{v}) - \underline{\nabla} \cdot (\psi \alpha \underline{v}) \right] d^3x$$

$$\int_{\mathbb{R}^3} \underline{\nabla} \cdot (\psi \alpha \underline{v}) d^3x = \int_{S(\mathbb{R}^3)} \alpha \psi \underline{v} \cdot \underline{n} dA = 0$$

Surface of  $\mathbb{R}^3$  is clearly outside  $V(t)$ ,  
so  $\psi = 0$  always

$$= \int_{\mathbb{R}^3} \psi \left[ \frac{\partial \alpha}{\partial t} + \underline{\nabla} \cdot (\alpha \underline{v}) \right] d^3x$$

$$= \int_{V(t)} \left[ \frac{\partial \alpha}{\partial t} + \underline{\nabla} \cdot (\alpha \underline{v}) \right] d^3x$$

$$= \int_{V(t)} \frac{\partial \alpha}{\partial t} d^3x + \int_{S(V(t))} \alpha \underline{v} \cdot \underline{n} d^2x$$

Using Gauss' theorem

Using the same method:

$$\frac{DI}{Dt} = \frac{D}{Dt} \left[ \int_V \alpha d^3x \right] = \frac{D}{Dt} \left[ \int_{\mathbb{R}^3} \alpha \psi d^3x \right] = \int_{\mathbb{R}^3} \frac{D}{Dt} (\alpha \psi) d^3x$$

$$= \int_{\mathbb{R}^3} \left[ \psi \frac{D\alpha}{Dt} + \alpha \frac{D\psi}{Dt} \right] d^3x = \int_V \frac{D\alpha}{Dt} d^3x$$

$$= \int_V \left( \frac{\partial \alpha}{\partial t} + \underline{\nabla} \cdot (\underline{v} \cdot \alpha) \right) d^3x = \int_V \frac{\partial \alpha}{\partial t} d^3x + \int_{S(V)} \alpha \underline{v} \cdot \underline{n} d^2x$$

## 4.1 Mass Conservation

Let  $\alpha = \rho$ , then  $I(t)$  is the total mass in the volume  $V$ :  $I = \int_V \rho dV = m$ . Assuming no mass is generated or annihilated within  $V$  and recalling that the volume/volume's area/surface is moving along with the fluid, we have  $\frac{DI}{Dt} = 0$

$$\Rightarrow \frac{DI}{Dt} = 0 = \int_V \frac{\partial \rho}{\partial t} dV + \int_A \underline{n} \cdot (\rho \underline{v}) dA$$

If  $V$  is now a fixed <sup>containing</sup> control volume:  $\int_V \frac{\partial \rho}{\partial t} dV = \frac{\partial}{\partial t} \int_V \rho dV$

$$\Rightarrow \frac{\partial}{\partial t} \int_V \rho dV = - \int_A \underline{n} \cdot (\rho \underline{v}) dA$$

## 4.2 Momentum Conservation

A control volume  $V$  with bounding surface  $A$  is chosen and the total momentum in  $V$  is given by

$$I(t) = \int_V \rho \underline{v} dV$$

Newton's law: The rate of change of the momentum in  $V$  is equal to the total force acting on  $V$ . The total force is divided into surface forces  $f_s$  and volume forces  $f_v$ :

$$f_s = \int_A \underline{S} dA, \quad f_v = \int_V \rho \underline{g} dV$$

$\underline{S}$ : stress vector, given in terms of stress tensor:  $\underline{S} = \underline{S} \cdot \underline{n}$

$\underline{g}$ : specific volume-force vector (inertial, gravitational, EM forces...)



This gives:  $\frac{DI}{Dt} = \int_S + \int_V$

$$\text{with } \alpha = \underline{SV}: \int_V \frac{\partial}{\partial t} (\underline{SV}) dV = - \int_A \underline{V} \cdot (\underline{n} \cdot \underline{SV}) dA + \int_S + \int_V$$

### 4.3 Conservation of Energy

The rate of change of total energy  $I = \int_V E dV$  is equal to the work done, per unit time, by all the forces acting on the volume plus the influx of energy per unit time into the volume.

A force  $\underline{f}$  acting on a point moving with velocity  $\underline{v}$  produces the work  $\underline{f} \cdot \underline{v}$  per unit time.

The surface and volume forces produce the following terms:

$$E_{\text{surf}} = - \int_A \underline{v} \cdot \underline{S} dA, \quad E_{\text{vol}} = \int_V \underline{S} (\underline{v} \cdot \underline{g}) dV$$

$$\text{Influx of energy: } E_{\text{influx}} = - \int_A (\underline{n} \cdot \underline{Q}) dA$$

Recall that the energy flow is given by the heat flux.

$$\Rightarrow \frac{DI(t)}{Dt} = E_{\text{surf}} + E_{\text{vol}} + E_{\text{influx}}$$

$$\Rightarrow \frac{d}{dt} \int_V E dV = - \int_A [\underline{S} \cdot \underline{v} + \underline{n} \cdot \underline{Q} - (\underline{n} \cdot \underline{E} \underline{v})] dA + \int_V \underline{S} (\underline{v} \cdot \underline{g}) dV$$

